

BETTER HEATING. SAFE BET.

TECHNICAL MANUAL DIAPHRAGM EXPANSION VESSELS

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Information to standards

Mentioned and quoted standards refer to the following versions:

	1	
•	EN 12828:2013-01-01	Heating systems in buildings - Design for water-based heating systems
•	ÖNORMH5151-1:2010-12-15	Planung von zentralen Warmwasser-Heizungsanlagen mit oder ohne Warmwasserbereitung - Teil 1
•	ÖNORM H 5155:2013-09-01	Wärmedämmung von Rohrleitungen und Komponenten in haustechnischen Anlagen
•	ÖNORM M 7777-2:2013-09-01	Solarthermische Anlagen - Teil 2

• EN ISO 4126-1:2013-10-15 Safety devices for protection against excessive pressure - Part 1: Safety valves

Disclaimer

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1.1 Operating principle and construction

Sealed diaphragm expansion vessels are safety devices for systems which use a liquid heat transfer medium - primarily water - to transport heat resp. cold to the particular loads.

A diaphragm expansion vessel consits of 2 champbers, which are divided by a high-quality membrane. In EDER expansion vessels this membrane is designed as a bag and encloses the medium completely. There is no contact between the medium and the metal wall of the vessel, thus corrosion is avoided.

The water chamber stores the change in water volume due to heating up. In case of cooling down the pressure inside the gas chamber presses the medium back to the system.

figure: expansion vessel in operation

Minimum system temperature The expansion vessel contains a water reserve. The system temperature rises The expansion vessel accomodates the incurring expansion volume inside the membrane. Maximum system temperature

The expansion vessel stores the expansion volume completely



1.2 The meaning of the gas pressure

A missing resp. incorrect set gas pressure affects the complete operation of the entire system.

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Therefore a individual inspection and adjustment of the gas pressure must be done prior to commissioning resp. once a year.

As mentioned above, the gas pressure shall ensure that the expansion volume is pressed back to the system in case of cooling down. Also it protects the vessel from overfilling.

If the gas pressure is missing or too small, the expansion vessel accomodates too much water at low system temperatures. In case of heating up, there is no room left for the physical expansion. Furthermore the durability of the expansion vessel is affected due to over-use of the membrane.

If the gas pressure is too high, the capacity of the vessel is reduced and the function of the system is disturbed too.

Due to the fact that the pressure in both chambers is equal, the expansion vessel must be pressure relieved when checking the gas pressure.

To check the gas pressure without draining the system, special armatures, so-called maintenance units, are available.

The gas pressure can be checked with a conventional tire-pressure gauge.

The necessary pressure within the gas chamber depends on the static height above the connection point of the expansion vessel.

If the temperature is above 100°C, the gas pressure must be increased by the value of the vapour pressure.

PRODUCT OVERVIEW

In this case the membrane must be protected from excessive temperature too.

After adjusting the gas pressure to the plant, the system can be filled to the adequate system pressure.

The detailed sizing procedure is described in Section 3.

figure: effect of the gas pressure



1.3 Application

The main applications of diaphragm expansion vessels are

• central heating systems

Eder

• climatic and cold water systems

2. Product overview

• solar systems

- drinking and service water systems
- water hammer arrestors
- etc.

heating, climatic and cold water systems heating, solar, cold water series series series series series series series NP SG С CV U -10 Ν U -6 3 bar 3 bar 3 bar 5 bar 10 bar 3 bar 6 bar solar systems sanitary systems refrigeration systems series series series series San D Cool Solar San 10 bar 10 bar 6 bar 6 bar

Better heating.



3. Sizing

The Sizing of expansion vessels is made according to relevant standards, for example EN 12828. A too small resp. incorrect sized expansion vessel affects the function of the system just as a incorrect set gas pressure.

If the expansion vessel is too small, it is unable to store the entire expansion volume.

In case of heating up, a part of the expansion volume gets lost via the system safety valve. When cooling down, this volume is missing and the pressure falls below its minimum value. Negative pressure arises and the system sucks air via various components (stuffing boxes, air vents etc.). Corrosion and circulation problems are the consequences.

To ensure a proper function, special attention must be paid to the correct sizing of the expansion vessel.

3.1 Safety expansion vessels for heating, climatic and cold water systems

3.1.1 hydraulic connection

example: elko-flex eder safety expansion vessel in hanging position



elko-flex eder safety expansion vessels for sealed systems are sized according to the standard EN 12828 "Heating systems in buildings".

A correct and sufficient sizing ensures a trouble-free operation of the system.

elko-flex eder safety expansion vessels store the temperature-dependent changes in water volume in sealed heating, climate and cold water systems with a maximum operating pressure of 3, 5, 6 resp. 10 bar and a maximum operating temperature of 90 °C (max. long-term temperature of the vessel is 70 °C). If the max. operating temperature is higher (max. 110 °C), an EV cooling

- 1... heating flow
- 2... heating return
- 3... expansion pipe
- 4 ... circulation pump
- 5 ... load
- 6 ... system safety valve
- 7 ... elko-flex eder maintenance unit
- 8 ... elko-flex eder safety expansion vessel
- h_{st} ... static height

vessel (compare "accessory") must be installed. This cooling vessel ensures an adequate cooling of the expansion volume before it gets into the expansion vessel.

According to ÖNORM H 5151-1 the use of more than one diaphragm expansion vessels must be avoided.

The recommended connection point of the safety expansion vessel is the (pressure-)neutral point in the pipe system. At this point the static resp. the final pressure is constant, independent from the operation of the circulation pumps. chosen in such a way that the pressure on the suction side of the circulation pump is sufficient for operation, e.g. avoiding cavitation, and high temperatures affecting the diaphragm of the expansion vessel.

The position of the integration point should be

3.1.2 Sizing of diaphragm expansion vessels according to EN 12828*:

* In Austria the standard ÖNORM H 5151-1 may also be applied as a supplement to EN 12828.

The size of the diaphragm expansion vessel depends on:

illustration of the different pressure levels:

- the total content of the system V_{System}
- the static height h_{st}
- the final pressure $p_{\mbox{\tiny fin}}$

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 the density ρ of the used medium, depending on the lowest and the maximum set operation temperature

Calculation of the **gas pressure (minimum operating pressure)** p_0 in the System:

 $p_0 = p_{st} + 0,2 + p_v$

- ϑ_{\min} lowest system temperature
- $\vartheta_{\scriptscriptstyle \mathsf{max}}$ maximum set system temperature
- p_{sv} set pressure of the safety value
- $p_{\mbox{\tiny PAZ}}$ pressure at which the pressure limiter operates.
- p_{fin} final pressure
- p_{fil} filling pressure required pressure in the system if the lowest possible temperature is not given. (for filling of make-up)
- p_{ini} initial pressure
- p₀ gas pressure (=minimum operating pressure, effectively avoiding evaporation, cavitation, vacuum)

In addition the minimum pressure requirements of other system components need to be taken into consideration. An addition of



at least 0,2 bar to the static height is recommended.

p_{st} static height pressure - pressure only resulting from the difference in height h_{st} between the position of the pressurization system and the highest point of the heating system.

10 meter water column (mWs) ~ 1 bar

- p_v vapour pressure at temperature θ_{max}
 Generally, specific values for the vapour pressure are values for pure water without any antifreeze additives (see table 3)
- V_{ex} expansion volume
- $V_{\ensuremath{\mathsf{WR}}}$ real water reserve volume in the pressure vessel used.
- operating band of the pressurization system



calculation example:

(sealed heating system with $\vartheta_{max} = 95 \text{ °C}$)

The water column above the expansion vessel is 7m. How large does the gas pressure p_0 have to be?

solution:

given: $h_{st} = 7 \text{ mWs} \rightarrow p_{st} = 0,7 \text{ bar}$ $p_v = 0 \text{ bar}$ asked for: p_0

 $p_0 = p_{st} + 0.2 + p_v = 0.7 + 0.2 + 0 = 0.9 \text{ bar}$

The gas pressure $p_{\scriptscriptstyle 0}$ within the vessel must be 0,9 bar.

Later the **total content of the system V**_{system} must be determined. It is the total content of the pipework, heat emitters, heat generators and connected auxiliary circuits. Where it is not feasible to make an accurate calculation, extra care should be taken in estimating the volume.

If the volumes of the individual components are unknown, the volume of the system can be determined approximately by using the nominal power of the heat generator and the plant-specific water content f_{an} (table 1).

 $V_{\text{System}} = f_{\text{an}} \times \Phi_{\text{NL}}$

 $\Phi_{_{\rm NL}}$ max. power of the heat generator [kW]

f_{an} plant-specific water content [1/kW] (table 1)

The **expansion volume** V_{ex} is the increase in volume caused by temperature increase between the lowest possible temperature of the heating system and the maximum set operating temperature of the heat generator.

 $V_{\mbox{\tiny ex}}$ is determined by using the expansion coefficiente:

$$V_{ex} = V_{System} x e$$
$$e = 1 - \frac{\rho_{9max}}{\rho_{9min}}$$

- $\rho_{\mbox{\tiny 9max}} \ \ \mbox{density of the medium at the maximum set} \\ operating temperature of the heat generator \\ [kg/m^3] (table 5)$
- $\begin{array}{ll} \rho_{\mbox{\tiny 9min}} & \mbox{density of the medium at the lowest system} \\ & \mbox{temperature} \, [\,kg/m^3] \, (table \, 5) \end{array}$

Note: The density of water (table 5) will be affected by the density of additive substances (e.g. antifreeze additives).

Usually the lowest system temperature is equal to the filling temperature of 10 °C.

Used additive substances can affect the material of the diaphragm!

calculation example:

How large is the expansion volume of a sealed heating system with convectors and a nominal power of $\Phi_{\rm NL}$ = 30 kW?

solution: given: $\Phi_{NL} = 30 \text{ kW}$ $f_{an} = 9 \text{ l/kW}$ (acc. to table 1) $\vartheta_{max} = 95 \text{ °C}$

asked for: V_{ex}

$$V_{system} = f_{an} \times \Phi_{NL} = 9 \times 30 = 270$$
 |

$$e = 1 - \frac{\rho_{\vartheta max}}{\rho_{\vartheta min}} = 1 - \frac{950,7}{999,7} = 4,9\%$$

 $V_{ex} = V_{System} x e = 270 x 4,9 \% = 13,231$

The expansion volume is 13,231.

In addition to the expansion volume, the expansion vessel should have a minimal water reserve.

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The water reserve V_{wR} compensates possible water losses in the system. Expansion vessels with a nominal volume up to 15 l should accommodate at least 20 % of this volume as a water reserve. Expansion vessels with a nominal volume greater than 15 l should accommodate a water reserve of at least 0,5 % of the total content of the system, however, at least 3 l.

$$\begin{split} V_{_{WR}} &= \frac{V_{_{N}} \times 20}{100} & \text{if } V_{_{N}} \leq 15 \text{ I} \\ \\ V_{_{WR}} &= \frac{V_{_{System}} \times 0,5}{100} \geq 3 & \text{if } V_{_{N}} > 15 \text{ I} \end{split}$$

 V_{WR} water reserve [1]

 V_N nominal volume of the expansion vessel [1] V_{System} total content of the system [1]

calculation example:

How large does the water reserve $V_{\mbox{\tiny WR}}$ have to be, if the total content of the heating system is 1.050 litres?

solution: given: $V_{System} = 1.050$ litres asked for: V_{WP}

Note: Due to the total content of the system it can be assumed that the nominal volume of the expansion vessel is greater than 15 litres!

$$V_{\rm WR} = \frac{V_{\rm System} \ge 0.5}{100} = \frac{1.050 \ge 0.5}{100} = \frac{5.251}{100}$$

The water reserve V_{WR} is 5,25 litres.

The **final pressure** \mathbf{p}_{fin} indicates the highest pressure in the operating range of the heating

system. It should not be higher than the set pressure of the safety valve minus a difference in shut-off overpressure, the so-called closing pressure difference p_{SD} .

According to EN ISO 4216-1 a closing pressure difference of 20%, at least 0,6 bar is admissible.

$$p_{\text{SD}} = p_{\text{SV}} \, x \, 20 \ \% \geqq 0,6 \text{ bar}$$

$$p_{\text{fin}} = p_{\text{SV}} - p_{\text{SD}}$$

 p_{SD} closing pressure difference [bar]

 p_{sv} set pressure of the safety value [bar]

p_{fin} final pressure [bar]

Note: The standard ÖNORM H 5151-1 specifies the closing pressure difference p_{sD} with 10% of the set pressure (blow-off pressure) P_{sv} of the safety valve, at least 0,5 bar.

Usually in Austria the **minimum set pressure of the safety valve** p_{sv} is defined with 2 bar above the static pressure p_{st} , at least 3 bar!

$$p_{sv} = p_{st} + 2 \ge 3 \text{ bar}$$

calculation example:

How large is the final pressure p_{fin} in a sealed heating system with a static height of 7 m?

solution:given: $h_{st} = 7 \text{ mWs} \rightarrow p_{st} = 0,7 \text{ bar}$ asked for: p_{fin}

 $p_{sv} = p_{st} + 2 = 0,7 + 2 = 2,7$ bar The minimum value is 3 bar $\rightarrow p_{sv} = 3$ bar

 $p_{fin} = p_{sv} - p_{sD} = 3 - 0,6 = 2.4 \text{ bar}$

The final pressure p_{fin} is 2,4 bar.

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Calculation of the **minimum nominal volume V**_{N,min} of diaphragm expansion vessels:

 $V_{_{N,min}} = (V_{_{ex}} + V_{_{WR}}) \ge \frac{p_{_{fin}} + 1}{p_{_{fin}} - p_{_0}}$

V_{N,min}minimum nominal volume [1]V_{ex}expansion volume [1]V_{WR}water reserve [1]p_{fin}final pressure [bar]p_0gas pressure [bar]

calculation example:

Calculate the necessary nominal volume $V_{N,min}$ and the gas pressure p_0 for a diaphragm expansion vessel in a system with a total content of $V_{System} = 320$ l and a static height of $h_{st} = 8$ mWs. The maximum operating temperature is $\vartheta_{max} = 95$ °C.

<u>solution:</u>

given:
$$V_{System} = 320 \text{ litres}$$

 $h_{st} = 8 \text{ mWs} \rightarrow p_{st} = 0.8 \text{ bar}$
 $\vartheta_{max} = 95 \text{ °C}$
asked for: $V_{N,min}$
 p_0

determination of the gas pressure p_0 : $p_0 = p_{st} + 0,2 + p_v = 0,8 + 0,2 + 0 = \underline{1 \text{ bar}}$

determination of the set pressure p_{sv} : $p_{sv} = p_{st} + 2 = 0.8 + 2 = 2.8$ bar The minimum value is 3 bar $\rightarrow p_{sv} = 3$ bar

determination of the final pressure p_{fin} : $p_{fin} = p_{sv} - p_{sD} = 3 - 0, 6 = 2,4$ bar

determination of the expansion volume V_{ex} :

$$e = 1 - \frac{\rho_{9max}}{\rho_{9min}} = 1 - \frac{961,7}{999,7} = 3,8\%$$
$$V_{ex} = V_{System} \times e = 320 \times 3,8\% = 12,21$$

determination of the water reserve V_{WR} : Due to the total content of the system it can be assumed that the nominal content of the expansion vessel is greater than 15 litres.

$$V_{\text{WR}} = \frac{V_{\text{System}} \times 0,5}{100} = \frac{320 \times 0,5}{100} = 1,61$$

The minimum value is $3 \downarrow \rightarrow V_{WR} = 3 \downarrow$

determination of $V_{N,min}$:

$$V_{N,min} = (V_{ex} + V_{WR}) \times \frac{p_{fin} + 1}{p_{fin} - p_0}$$
$$V_{N,min} = (12, 2 + 3) \times \frac{2, 4 + 1}{2, 4 - 1} = \underline{36, 81}$$

The required expansion vessel has to have a minimum nominal volume of 36,8 litres.

During commissioning the gas pressure must be set to 1,0 bar.

Selection and correct sizing of the diaphragm expansion vessel:

 $V_{_{N}} \geqq V_{_{N,min}}$

For diaphragm expansion vessels the initial pressure p_{ini} shall be confirmed for the selected vessel as follows:

$$p_{ini} = \frac{p_{fin} + 1}{1 + \frac{V_{ex}}{V_N} \times \frac{p_{fin} + 1}{p_0 + 1}} - 1$$

The correct sizing of the expansion vessel is ensured as long as:

 $p_{\text{ini}} \geqq p_{\text{0}}$ + 0,3 bar

Otherwise the nominal volume $V_{\scriptscriptstyle N}$ should be increased until the condition above is met.

calculation example:

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Using the determined nominal volume, the expansion vessel can be selected from the tables in section "technical data".

It should be noted that the next larger expansion vessel must be selected!

<u>solution:</u>

given: $V_{N,min} = 36,81$ asked for: appropriate expansion vessel

\rightarrow selected vessel: <u>elko-flex eder N</u>	<u>50</u>
nominal volume V_{N} :	50 litres
max. operating pressure:	3bar
max. long-term temperature:	70°C

$$p_{ini} = \frac{p_{fin} + 1}{1 + \frac{V_{ex}}{V_N} \times \frac{p_{fin} + 1}{p_0 + 1}} - 1$$
$$p_{ini} = \frac{2.4 + 1}{1 + \frac{12.2}{50} \times \frac{2.4 + 1}{1 + 1}} - 1 = 1.41 \text{ bar}$$

 $p_{_{ini}} \geqq p_{_0} + 0,3 \text{ bar}$

$$\mathsf{p}_{\mathsf{ini}} \geqq \mathsf{1} + \mathsf{0}, \mathsf{3} \mathsf{ bar} = \mathsf{1}, \mathsf{3} \mathsf{ bar}$$

The required term is fulfilled, the selected elko-flex eder N50 can be used.

Note: According to ÖNORM H 5151-1 a pumpcontrolled pressurization device is state of the art in larger systems (nominal power 100 kW and higher, total content 5000 litres and higher or 100 m² solar collector area).

The nominal volume $V_{\mbox{\tiny N,min}}$ of these expansion vessels is determined as follows (acc. to EN 12828):



η utilisation efficiency of the expansion vessel (at pressureless elko-mat eder expansion vessels \rightarrow η = 100 %) The **filling pressure** \mathbf{p}_{fil} is the required pressure in the system if the lowest possible temperature ϑ_{min} is not given (for filling of water make-up).

$$p_{\text{fil}} = V_{\text{N}} x \frac{p_{\text{o}} + 1}{V_{\text{N}} - V_{\text{System}} x \left(1 - \frac{\rho_{\text{9fil}}}{\rho_{\text{9min}}}\right) - V_{\text{WR}}} - 1$$

- p_{fil} filling pressure [bar]
- p_0 gas pressure [bar]
- V_{N} nominal volume of the expansion vessel [1]
- V_{System} total content of the system [1]
- $V_{_{WR}} \quad water\, reserve\, [\,m^3\,]$
- $\rho_{\mbox{\tiny 9fil}} \ \ \, density of the medium at the current system temperature during fill or make-up process [kg/m^3](table 5)$
- $\begin{array}{ll} \rho_{\mbox{\tiny 9min}} & \mbox{density of the medium at the lowest system} \\ & \mbox{temperature} \, [\,kg/m^3\,] \, (table \, 5) \end{array}$

calculation example:

Determine the filling pressure $p_{\mbox{\tiny fil}}$ for the above mentioned system.

solution:

given:
$$p_0 = 1$$
 bar
 $V_N = 50$ litres
 $V_{System} = 320$ litres
 $V_{WR} = 3$ litres
current system temp. = 60 °C
asked for: filling pressure p_{G} of the system

$$\vartheta_{fil} = 60 \degree C$$

 $\rightarrow \rho_{\vartheta fil} = 983,1 \text{ kg/m}^3$

$$p_{\text{fil}} = V_{\text{N}} \times \frac{p_{\text{o}} + 1}{V_{\text{N}} - V_{\text{System}} \times (1 - \frac{\rho_{\text{Bfil}}}{\rho_{\text{Bmin}}}) - V_{\text{WR}}} - 1$$

$$p_{fil} = 50 \times \frac{1+1}{50 - 320 \times (1 - \frac{983,1}{999,7}) - 3} - 1$$

$$p_{fil} = 1,24 \text{ bar}$$

The filling pressure p_{fil} is 1,24 bar.

In ÖNORM H 5151-1 the filling pressure p_a is determined as follows:

To ensure that the diaphragm expansion vessel can accommodate the water reserve in the cold state of the system, the filling pressure must be at least equal to the value $p_{a,min}$:

$$p_{a,min} = \frac{V_{N} x (p_{v} + 1)}{V_{N} - V_{v}} - 1$$

 $\begin{array}{ll} p_v & \mbox{relative gas pressure (p_{st} + 0.3 \geqq 1.0 \mbox{ bar)} \\ V_v & \mbox{water reserve} & \triangleq V_{_{W\!R}} \mbox{ in EN 12828} \end{array}$

The filling pressure must not exceed the value $p_{\text{a,max}}\!\!:$

$$p_{a,max} = \frac{p_e + 1}{1 + \frac{V_e x (p_e + 1)}{V_N x (p_V + 1)}} - 1$$

- p_{e} final pressure $\triangleq p_{fin}$ in EN 12828
 - expansion volume $riangleq V_{ex}$ in EN 12828
- p_v relative gas pressure (p_{st} + 0,3 \geq 1,0 bar)

The filling pressure must be confimed with the following term:

 $p_{\text{a,max}} \geqq p_{\text{a,min}} + 0,2$

٧_°

 $p_{a,max}$ max. filling pressure of the cold system $p_{a,min}$ min. filling pressure of the cold system

If this term is not fulfilled, the next larger expansion vessel must be selected and confirmed.

Note: The real filling pressure of the system should be between the minimum filling pressure $p_{a,min}$ and the maximum filling pressure $p_{a,max}$.

The correct and adequate sizing is essential for a problem-free function of the system.

3.1.3 Sizing of the expansion pipe

SIZING

acc. to ÖNORM H 5151-1:

The following point must be considered:

• To determine the dimension of the expansion pipe the nominal power of the heat generator must be known.

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- For systems with a nominal power lower than 500 kW the minimum dimensions can be taken from table 2.
- The maximum flow rate within the expansion pipe must not exceed 0,15 m/s.

Note for the insulation of the expansion pipe:

According to ÖNORM H 5155 expansion pipes must only be insulated up to 10 cm from the connection to the system return.



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3.2 Expansion vessels for warm water sanitary systems

elko-san eder San D series expansion vessels are mainly used in sealed warm water sanitary systems.

They prevent opening and thus the crusting of the safety valves during preparation of warm water, precious water can't get lost during heating-up.

Due to the special construction the water can flow through the vessel. Therefore the increasing hygienic requirements get fulfilled. The diaphragm is made of food-safe and tasteless material, connection and flange are made of stainless steel.

An adequate sizing ensures the compliance of the points mentioned above and guarantees a problem-free operation.

To calculate an elko-san eder San D series expansion vessel the following technical specifications of the systems are necessary:

- volume of the water boiler
- max. warm water temperature
- inlet pressure (=set pressure of the pressure reducing valve)
- set pressure of the safety valve

The adjoining diagrams can be used to simplify the sizing of elko-san eder San D expansion vessels.

The diagrams are based on a gas pressure of 0,2 bar lower than the idle pressure of the water supply. The reduced volume of the vessel, caused by the water reserve resp. expansion factors acc. to standard is already considered.

After sizing and selection of the expansion vessel the relevant accessory can be selected.

Caution: elko-san eder San D expansion vessels are installed to the system via 2 pcs. elko-flex eder maintenance units. The gas pressure (acc. to the calculation) must be set during commissioning.



selection diagram 1

set pressure of the safety valve:6 barinlet pressure (press. reducing valve):3,7 bargas pressure within the expansion vessel:3,5 bar



selection diagram 2

set pressure of the safety valve:	6bar
inlet pressure (press. reducing valve):	2,7 bar
gas pressure within the expansion vessel:	2,5 bar





3.3 Safety expansion vessels for refrigeration systems

elko-flex eder Cool series safety expansion vessels are designed to use in refrigeration systems (cold water systems, chillers)

The diaphragms are resistant to common antifreeze fluids based on glycol. The connection flange is made of stainless steel.

3.3.1 hydraulic connection

elko-flex eder Cool series safety expansion vessels are designed for wall mounting. Generally the vessel is installed with the connection on the bottom and a pipe loop to the system return. Thus the diaphragm is protected against too cold temperatures in refrigeration systems.

The operating temperature of elko-flex eder Cool safety expansion vessels is between -10 °C und +70 °C. Outside of this range the vessel must be protected with an EV cooling vessel.

The expansion pipe must be installed in a way that no cushion air can be enclosed. Otherwise a proper venting device must be installed. To ensure maintenance without emptying the system, the vessel must be installed with a maintenance unit.

example: elko-flex eder Cool



- 1... system flow
- 2... system return
- 3... expansion pipe
- 4... circulation pump
- 5... load
- 6... safety valve
- 7 ... elko-flex eder maintenance unit
- 8... elko-flex eder Cool safety expansion vessel

3.3.2 Sizing of safety expansion vessels for refrigeration systems*:

* sizing follows EN 12828.

An adequate sizing of the expansion vessel ensures the compliance with the pressure limits over the entire temperature range and guarantees a problem-free operation.

Depending on situation and type of the elko-flex eder Cool expansion vessel the volume must be calculated in a way that the maximum operating pressure does not exceed at the maximum operating temperature. Also unwanted low pressure must be avoided in case of too low temperatures (e.g. negative temperatures). To calculate an elko-flex eder Cool series safety expansion vessel the following technical specifications of the system are necessary:

- total content of the refrigeration system V_{System}[1]
- max. ambient temperature 9_{max}, which can occur at standstill of the cold generator [°C]
- min. temperature 9_{min} in the refrigeration system, corresponds to the lowest flow temperature of the cold generator [°C]
- static height pressure p_{st} [mWs]
- max. operating pressure p_{sv} of the system [bar]

The correct **gas pressure** \mathbf{p}_0 (=minimum operating pressure) avoids low pressure (with the result of diffusion etc.) in low temperature situations of normal operating systems. Therefore an addition to the static height pressure p_{st} should be considered preventively, whereby the minimum operating pressure is higher than necessary.

$p_0 = p_{st} + 0,2$

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- p_0 min. operating pressure = gas pressure [bar]
- p_{st} static height pressure pressure only resulting from the difference in height h_{st} between the position of the pressurization system and the highest point of the refrigeration system

10 meter water column (mWs) ~ 1 bar

$\label{eq:calculation} Calculation of the \ expansion \ volume \ V_{\mbox{\tiny ex}} :$



- e expansion coefficient
- $\begin{array}{ll} \rho_{\mbox{\tiny 9max}} & \mbox{density of the medium (e.g. water/antifreeze} \\ & \mbox{mix) at ambient temperature [kg/m^3] (table 5) \end{array}$
- $\rho_{\mbox{\tiny 9min}} \ \ \mbox{density of the medium at the lowest flow} \\ temperature [kg/m^3] (table 5)$

Used additive substances can affect the material of the diaphragm!

Calculation of the water reserve $V_{\mbox{\tiny WR}}$:

$$\begin{split} V_{_{WR}} &= \frac{V_{_{N}} \times 20}{100} & \text{if } V_{_{N}} \leq 15 \text{ I} \\ V_{_{WR}} &= \frac{V_{_{System}} \times 0.5}{100} \geq 3 & \text{if } V_{_{N}} > 15 \text{ I} \end{split}$$

 V_{WR} water reserve [1]

 V_{N} nominal volume of the expansion vessel [1] V_{system} total content of the system [1]

Usually in Austria the **minimum set pressure of the safety valve** p_{sv} is defined with 2 bar above the static pressure p_{sv} , at least 3 bar!

 $p_{sv} = p_{st} + 2 \ge 3 \text{ bar}$

The **final pressure** p_{fin} indicates the highest pressure in the operating range of the refrigeration system. It should not be higher than the set pressure of the safety valve minus a difference in shut-off overpressure, the so-called closing pressure difference p_{sD} .

According to EN ISO 4216-1 a closing pressure difference of 20%, at least 0,6 bar is admissible.

$$p_{\text{SD}} = p_{\text{SV}} \, x \, 20 \ \% \geqq 0,6 \text{ bar}$$

$$p_{\text{fin}} = p_{\text{SV}} - p_{\text{SD}}$$

- p_{SD} closing pressure difference [bar]
- $p_{sv} \quad set \, pressure \, of the \, safety \, valve \, [\, bar \,]$
- p_{fin} final pressure [bar]

Note: The standard ÖNORM H 5151-1 specifies the closing pressure difference p_{SD} with 10% of the set pressure (blow-off pressure) of the safety valve, at least 0,5 bar.

Calculation of the **minimum nominal volume V**_{N,min} of diaphragm expansion vessels:

$$V_{N,min} = (V_{ex} + V_{WR}) \times \frac{p_{fin} + 1}{p_{fin} - p_0}$$

 $V_{N,min}$ minimum nominal volume [1]

- V_{ex} expansion volume [1]
- V_{WR} water reserve [1]
- p_{fin} final pressure [bar]

 p_0 gas pressure [bar]

Selection and correct sizing of the diaphragm expansion vessel:



For diaphragm expansion vessels the initial pressure p_{ini} shall be confirmed for the selected vessel as follows:

$$p_{ini} = \frac{p_{fin} + 1}{1 + \frac{V_{ex}}{V_N} \times \frac{p_{fin} + 1}{p_0 + 1}} - 1$$

The correct sizing of the expansion vessel is ensured as long as:

$$\mathsf{p}_{_{\mathsf{ini}}} \geqq \mathsf{p}_{_{\mathsf{0}}} + \mathsf{0,3}\,\mathsf{bar}$$

Otherwse the nominal volume $V_{\scriptscriptstyle N}$ should be increased until the condition above is met.

During **filling of cold water systems** special attention must be paid to the current operating mode of the system. It must be differentiated whether the system gets filled for the first time or a make-up process takes place (e.g. during maintenance).

Calculation of the **filling pressure** \mathbf{p}_{fil} for the first fill of a cold water system:

$$p_{\text{fil}} = V_{\text{N}} x \frac{p_{\text{o}} + 1}{V_{\text{N}} - V_{\text{System}} x \left(1 - \frac{\rho_{\text{9fil}}}{\rho_{\text{9min}}}\right) - V_{\text{WR}}} - 1$$

- $p_{_{fil}} \quad \ filling\, pressure\, [\,bar\,]$
- p_0 gas pressure [bar]
- $V_{\scriptscriptstyle N} ~~ {\rm nominal\,volume\,of\,the\,expansion\,vessel\,[1]}$
- V_{System} total content of the system [1]
- V_{WR} water reserve [m³]
- $\begin{array}{ll} \rho_{\mbox{\tiny BFI}} & \mbox{density of the medium at filling temperature} \\ & \mbox{[kg/m^3](table 5)*} \end{array}$
- $\rho_{\mbox{\tiny 9min}}$ density of the medium at the lowest flow temperature [kg/m³] (table 5)

* If the system gets filled with water, the filling temperature is 10 °C (in general). Depending on the storage temperature of the added antifreeze fluid the temperature of the medium could be higher. Calculation of the **filling pressure p**_{erg} for make-up (=**supplement pressure**):

$$p_{\text{erg}} = V_{\text{N}} x \frac{p_{\text{o}} + 1}{V_{\text{N}} - V_{\text{System}} x \left(1 - \frac{\rho_{\text{9erg}}}{\rho_{\text{9min}}}\right) - V_{\text{WR}}} - 1$$

- p_{erg} filling pressure (=supplement pressure) [bar]
- p_0 gas pressure [bar]
- V_{N} nominal volume of the expansion vessel [1]
- V_{System} total content of the system [1]
- V_{WR} water reserve [m³]
- $\begin{array}{ll} \rho_{\scriptscriptstyle \vartheta erg} & \mbox{density of the medium at the current system} \\ & \mbox{temperature during make-up process} \\ & \mbox{[kg/m^3](table 5)} \end{array}$
- $\rho_{\mbox{\tiny 9min}} \ \ \mbox{density of the medium at the lowest flow} \\ temperature [kg/m^3] (Tabelle 5)$

calculation example:

Calculate the appropriate diaphragm expansion vessel for a refrigeration system:

<u>solution:</u>

given:	$h_{st} = 2 \text{ mWs} \rightarrow p_{st} = 0.2 \text{ bar}$
	$V_{\text{System}} = 280 \text{ litres}$
	ethylene glycol 34 % (up to -20 °C)
	$\vartheta_{max} = 30 \ ^{\circ}C$
	$\vartheta_{min} = -10 \ ^{\circ}C$
	$p_{sv} = 3 bar$
asked for:	appropriate expansion vessel
	filling pressure for first fill
	filling pressure for make-up

 $p_0 = p_{st} + 0.2 = 0.2 + 0.2 = 0.4 \rightarrow set 1 bar$

$$e = 1 - \frac{\rho_{\vartheta max}}{\rho_{\vartheta min}} = 1 - \frac{1045}{1064} = 1.8 \%$$

$$V_{ex} = V_{System} \times e = 280 \times 0,018 = 5,04$$

$$V_{\text{WR}} = \frac{V_{\text{System}} \ge 0.5}{100} \ge 3$$

$$V_{WR} = \frac{280 \times 0.5}{100} = 1.4 \mid \rightarrow V_{WR} = 3 \mid$$

 $p_{SV} = p_{st} + 2$ = 0,2 + 2 = 2,2 \rightarrow set: $p_{SV} = 3$ bar $p_{SD} = p_{SV} \times 20 \% \ge 0,6$ bar = 3 x 0,2 = 0,6 \rightarrow $p_{SD} = 0,6$ bar $p_{fin} = p_{SV} - p_{SD} = 3 - 0,6 = 2,4$ bar $V_{N,min} = (V_{ex} + V_{WR}) \times \frac{p_{fin} + 1}{p_{fin} - p_{0}}$ $V_{N,min} = (5,04 + 3) \times \frac{2,4 + 1}{2,4 - 1} = \underline{19,51}$

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→ selected vessel: <u>elko-flex eder Cool 25</u> nominal volume V_N : 25 litres max. operating pressure: 6 bar max. long-term temperature: 70 °C

$$p_{ini} = \frac{p_{fin} + 1}{1 + \frac{V_{ex}}{V_N} \times \frac{p_{fin} + 1}{p_0 + 1}} - 1$$

$$p_{ini} = \frac{2.4 + 1}{1 + \frac{5.04}{25} \times \frac{2.4 + 1}{1 + 1}} - 1 = 4,15 \text{ bar}$$

 $p_{ini} \ge p_0 + 0,3 \text{ bar}$ $p_{ini} \ge 1 + 0,3 \text{ bar} = 1,3 \text{ bar}$

The required term is fulfilled, the selected elko-flex eder Cool 25 can be used.

matching maintenance unit: elko-flex eder maintenance unit 3/4" a/i

For the first fill of the cold water system, the used medium is a water/antifreeze mix with 34 % ethylene glycol, the storage temperature is $\vartheta_{fil} = 20 \text{ °C} \rightarrow \rho_{sfil} = 1050 \text{ kg/m}^3$

$$p_{\text{fil}} = V_{\text{N}} \times \frac{p_{\text{o}} + 1}{V_{\text{N}} - V_{\text{System}} \times \left(1 - \frac{\rho_{\text{sfil}}}{\rho_{\text{smin}}}\right) - V_{\text{WR}}} - 1$$

$$= 25 \times \frac{1+1}{25 - 280 \times (1 - \frac{1050}{1064}) - 3} - 1$$

 $p_{fil} = 1,73 bar$

The necessary filling pressure for first fill is 1,73 bar.

asked for: Filling pressure for make-up during annual maintenance.

During maintenance the average temperature of the cold water system is $\vartheta_{erg} = -5 \text{ °C} \rightarrow \rho_{\vartheta erg} = 1062 \text{ kg/m}^3$

$$p_{erg} = V_{N} \times \frac{p_{0} + 1}{V_{N} - V_{System} \times (1 - \frac{\rho_{\vartheta erg}}{\rho_{\vartheta min}}) - V_{WR}} - 1$$
$$= 25 \times \frac{1 + 1}{25 - 280 \times (1 - \frac{1062}{1064}) - 3} - 1$$
$$p_{erg} = \underline{1.33 \text{ bar}}$$

The necessary filling pressure for make-up p_{erg} (=supplement pressure) is 1,33 bar

Note: According to ÖNORM H 5151-1 a pumpcontrolled pressurization device is state of the art in larger systems (nominal power 100 kW and higher, total content 5000 litres and higher or 100 m² solar collector area)

The nominal volume $V_{N,min}$ of these expansion vessels is determined as follows (acc. to EN 12828):

$$V_{_{N,min}} = (V_{_{ex}} + V_{_{WR}}) \times \frac{1}{\eta}$$

η utilisation efficiency of the expansion vessel (at pressureless elko-mat eder expansion vessels \rightarrow η = 100 %)

EDEL

calculation example:

Calculate the correct expansion vessel for a cold water system. The static height of the system is 12 mWs, the system is filled with 450 litres of water.

The flow temperature of the system is 5 °C, the ambient temperature is 30 °C.

solution:

given: $h_{st} = 12 \text{ mWs} \rightarrow p_{st} = 1,2 \text{ bar}$ $V_{System} = 450 \text{ litres}$ $\vartheta_{max} = 30 \text{ °C}$ $\vartheta_{min} = 5 \text{ °C}$ asked for: appropriate expansion vessel filling pressure for first fill

filling pressure für make-up

$$p_0 = p_{st} + 0,2 = 1,2 + 0,2 = 1,4 \rightarrow set 2 bar$$

$$e = 1 - \frac{\rho_{\vartheta max}}{\rho_{\vartheta min}} = 1 - \frac{995,7}{999,9} = 0,4 \%$$

$$V_{ex} = V_{System} \times e = 230 \times 0,004 = 1,81$$

$$V_{WR} = \frac{V_{System} \ge 0.5}{100} \ge 3$$
$$V_{WR} = \frac{450 \ge 0.5}{100} = 2,25 \mid \rightarrow V_{WR} = 3 \mid$$

 $p_{\scriptscriptstyle SV} = p_{\scriptscriptstyle st} + 2$

= 1,2 + 2 = 3,2 → set: p_{sv} = 6 bar

 $p_{\scriptscriptstyle SD}$ = $p_{\scriptscriptstyle SV}\,x$ 20 % \geqq 0,6 bar

$$= 6 \times 0.2 = 1.2 \rightarrow p_{SD} = 1.2 \text{ bar}$$

$$p_{\mbox{\tiny fin}}=p_{\mbox{\tiny SV}}$$
 - $p_{\mbox{\tiny SD}}=6$ - 1,2 = 4,8 bar

$$V_{\text{N,min}} = (V_{\text{ex}} + V_{\text{WR}}) \times \frac{p_{\text{fin}} + 1}{p_{\text{fin}} - p_{0}}$$

$$V_{N,min} = (1,8+3) \times \frac{4,8+1}{4,8-1} = \frac{7,33 \text{ I}}{7,33 \text{ I}}$$

→ selected vessel: <u>elko-flex eder Cool 18</u> nominal volume V_N : 18 litres

$$\begin{split} p_{ini} &= \frac{p_{fin}+1}{1+\frac{V_{ex}}{V_N}} \cdot \frac{p_{fin}+1}{p_0+1} - 1 \\ p_{ini} &= \frac{4,8+1}{1+\frac{7,33}{18}} \cdot \frac{4,8+1}{1+1} - 1 = 1,66 \text{ bal} \\ p_{ini} &\geq p_0 + 0,3 \text{ bar} = 1 + 0,3 = 1,3 \text{ bar} \end{split}$$

The required term is fulfilled, the selected elko-flex eder Cool 18 can be used.

The cold water system is filled with water with a filling temperature of $\vartheta_{fil} = 10 \text{ °C}$ $\rightarrow \rho_{gfil} = 999,8 \text{ kg/m}^3$

$$p_{fil} = V_N \times \frac{p_0 + 1}{V_N - V_{System} \times (1 - \frac{\rho_{9fil}}{\rho_{9min}}) - V_{WR}} - 1$$
$$= 18 \times \frac{2 + 1}{18 - 450 \times (1 - \frac{999,8}{999,9}) - 3} - 1$$
$$p_{fil} = 2.61 \text{ bar}$$

The necessary filling pressure for first fill is 2,61 bar.

The make-up happens in deactivated status of the cold water system. At that time the average system temperature is $\vartheta_{erg} = 15 \text{ °C}$ $\rightarrow \rho_{\vartheta_{erg}} = 999,2 \text{ kg/m}^3$

$$p_{erg} = V_{N} \times \frac{p_{0} + 1}{V_{N} - V_{System} \times (1 - \frac{\rho_{9erg}}{\rho_{9min}}) - V_{WR}} - 1$$
$$= 18 \times \frac{2 + 1}{18 - 450 \times (1 - \frac{999, 2}{999, 9}) - 3} - 1$$

p_{erg} = <u>2,68 bar</u>

The necessary filling pressure for make-up p_{era} (=supplement pressure) is 2,68 bar

3.4 Safety expansion vessels for solar systems

elko-flex eder Solar series safety expansion vessels are designed to use in solar systems.

The diaphragms are resistant to common antifreeze fluids based on glycol. The connection flange is made of stainless steel.

3.4.1 hydraulic connection

EDEL

Depending on type and construction of the elko-flex eder Solar safety expansion vessel, it must be mounted to the wall (up to Solar 60) or to the ground (Solar 90 and higher).

Generally the vessel is installed with the connection on the bottom and a pipe loop to the system return. Thus the vessel is protected against too high temperatures which affect the lifetime of the diaphragm.

The maximum long-term temperature of the diaphragm is 70 °C. If the temperature can exceed, the vessel must be protected with an EV cooling vessel.

The expansion pipe must be installed in a way that no cushion air can be enclosed. Otherwise a

proper venting device must be installed.

To ensure maintenance without emptying the system, the vessel must be installed with a maintenance unit.

example: elko-flex eder Solar safety expansion vessel in hanging position



9... warm water boiler

3.4.2 Sizing of diaphragm expansion vessels for solar systems*:

* sizing follows EN 12828.

An adequate sizing of the expansion vessel ensures the compliance with the pressure limits over the entire temperature range and guarantees a problem-free operation.

Depending on the situation and type of the elkoflex eder Solar expansion vessel the volume must be calculated in a way that the maximum operating pressure does not exceed at the maximum operating temperature. Also unwanted low pressure must be avoided in case of too low temperatures (e.g. negative temperatures). To calculate an elko-flex eder Solar series safety expansion vessel the following technical specifications of the system are necessary:

- total content of the solar system V_{System}[1]
- total content of the collector $V_{\kappa}[1]$
- max. standstill temperature [°C]

6... collector

- max. temperature \u03c8_{max}, to prevent the content of the collector from evaporating [°C]
- static height pressure p_{st}[mWs]
- max. operating pressure p_{sv} of the system [bar]

The correct **gas pressure** p_0 (=minimum operating pressure) avoids evaporating of the medium in normal operating mode of the solar system. Also it avoids low pressure (with the result of diffusion etc.) during cooling down and at standstill of the system in winter.

$p_0 = p_{st} + 0,2 + p_v$

- p₀ min. operating pressure = gas pressure (effectively avoiding evaporation, cavitation, vacuum) = nominal inlet pressure of the pressurization system[bar]
- p_{st} static height pressure pressure only resulting from the difference in height h_{st} between the position of the pressurization system and the highest point of the solar system

10 meter water column (mWs) ~ 1 bar

p_v vapour pressure [bar] at temperature θ_{max}
 Specific values for common antifreeze fluids are specified in table 3

Calculation of the expansion volume V_{ex} :



- e expansion coefficient
- ρ_{smax} density of the medium (e.g. water/antifreeze mix) at the maximum temperature before evaporation [kg/m³] (table 5)
- $\rho_{\mbox{\tiny 9min}}$ density of the medium at filling temperature $[kg/m^3]$ (table 5)

Usually the filling temperature is specified with 10 $^{\circ}\mathrm{C}.$

Used additive substances can affect the material of the diaphragm!

Calculation of the water reserve V_{wR} :

$$\begin{split} V_{\text{WR}} &= \frac{V_{\text{N}} \times 20}{100} & \text{if } V_{\text{N}} \leq 15 \text{ I} \\ \\ V_{\text{WR}} &= \frac{V_{\text{System}} \times 0.5}{100} \geq 3 & \text{if } V_{\text{N}} > 15 \text{ I} \end{split}$$

 V_{WR} water reserve [1]

 V_N nominal volume of the expansion vessel [1] V_{System} total content of the system [1]

Usually the **minimum set pressure of the safety valve** p_{sv} is defined with 2 bar above the static pressure p_{st} , at least 3 bar!

 $p_{sv}=p_{\scriptscriptstyle 0}+2\geqq 3\,bar$

The **final pressure** p_{fin} indicates the highest pressure in the operating range of the solar system. It should not be higher than the set pressure of the safety valve minus a difference in shut-off overpressure, the so-called closing pressure difference p_{SD} .

According to EN ISO 4216-1 a closing pressure difference of 20%, at least 0,6 bar is admissible.

$$p_{\text{SD}} = p_{\text{SV}} \, x \, 20 \ \% \ge 0,6 \text{ bar}$$

$$p_{\text{fin}} = p_{\text{SV}} - p_{\text{SD}}$$

- p_{SD} closing pressure difference [bar]
- p_{sv} set pressure of the safety valve [bar]
- p_{fin} final pressure [bar]

Note: The standard ÖNORM H 5151-1 specifies the closing pressure difference with 10 % of the set pressure (blow-off pressure) P_{sv} of the safety valve, at least 0,5 bar.

Calculation of the **minimum nominal volume V** $_{N,min}$ of diaphragm expansion vessels:

It must be considered, that the content of the collector (or at least a part of it) can be heated to

the standstill temperature of the collector. The

EDEL

standstill temperature depends on the collector and can exceed 160 °C, it must be requested from the manufacturer.

Due to this high temperatures, the content of the collector can evaporate, thus the medium is protected against further rising temperatures.

Note: Most antifreeze fluids based on propylene glykol are suitable for long-term temperatures of max. 170 °C. Higher temperatures result in faster aging and thermal decomposition of the antifreeze fluid.

Therefore expansion vessels must be sized big enough to accommodate the content of the collector $V_{\kappa}\!\!:$

$$V_{\text{N,min}} = \left(V_{\text{ex}} + V_{\text{K}} + V_{\text{WR}}\right) \times \frac{p_{\text{fin}} + 1}{p_{\text{fin}} - p_{0}}$$

- V_{ex} expansion volume [1]
- $V_{\kappa} \quad \ \ total \ \ content \ \ of \ the \ \ collector \ (as \ \ declared \ by \ \ the \ \ manufacturer \ \ of \ the \ \ collector)[1]$

 V_{WR} water reserve [1]

 p_{fin} final pressure [bar]

 p_0 gas pressure [bar]

If the expansion vessel is sized too small, the system pressure exceeds the set pressure of the safety valve. The safety valve opens and medium gets lost. During cooling down this medium is missing, diffusion would be the consequence.

Selection and correct sizing of the diaphragm expansion vessel:



For diaphragm expansion vessels the initial pressure p_{ini} shall be confirmed for the selected vessel as follows:



The correct sizing of the expansion vessel is ensured as long as:



Otherwise the nominal volume $V_{\scriptscriptstyle N}$ should be increased until the condition above is met.

Calculation of the **filling pressure** \mathbf{p}_{fil} of the solar system in cold state:

$$p_{\text{fil}} = V_{\text{N}} x \frac{p_{\text{o}} + 1}{V_{\text{N}} - V_{\text{System}} x \left(1 - \frac{\rho_{\text{sfil}}}{\rho_{\text{smin}}}\right) - V_{\text{WR}}} - 1$$

- $p_{_{fil}} \quad \ filling\, pressure\, [\,bar\,]$
- p_0 gas pressure [bar]
- V_{N} nominal volume of the expansion vessel [1]
- V_{System} total content of the system [1]

 V_{WR} water reserve [m³]

- $ho_{\mbox{\tiny BFI}}$ density of the medium at the current system temperature during fill or make-up process [kg/m³](table 5)
- $\rho_{\text{\tiny 9min}} \quad \text{density of the medium at the lowest system} \\ \text{temperature} [kg/m^3] (table 5)$

calculation example:

Calculate the appropriate diaphragm expansion vessel for a solar system:

solution:

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given:	$h_{st} = 12 \text{ mWs} \rightarrow p_{st} = 1.2 \text{ bar}$
	$V_{System} = 37$ litres
	$V_{\kappa} = 18$ litres
	propylene glycol 39 % (-20 °C)
	evaporation at 120 °C
asked for:	appropriate expansion vessel

$p_0 = p_{st} + 0.2 + p_v = 1.2 + 0.2 + 0.74 = 2.14$ bar $e = 1 - \frac{\rho_{\text{9max}}}{\rho_{\text{9min}}} = 1 - \frac{973}{1042} = 6.6 \%$ $V_{ex} = V_{System} \times e = 37 \times 0,066 = 2,44$ | $V_{\text{WR}} = \frac{V_{\text{System}} \times 0.5}{100} \ge 3$ $V_{_{WR}} = \frac{37 \times 0.5}{100} = 0.19 \mid \rightarrow V_{_{WR}} = 3 \mid$ $p_{sv} = p_0 + 2$ $p_{sv} = 2,14 + 2 = 4,14$ bar \rightarrow set: $p_{sv} = 6$ bar $p_{fin} = p_{SV} \times 0.8 = 6 \times 0.8 = 4.8 \text{ bar}$ $V_{N,min} = (V_{ex} + V_{K} + V_{WR}) \times \frac{p_{fin} + 1}{p_{fin} - p_{0}}$ $V_{N,min} = (2,44 + 18 + 3) \times \frac{4,8 + 1}{4.8 - 2.14} = \frac{51,11}{2.14}$ → selected vessel: <u>elko-flex eder U60-10</u> nominal volume V_N: 60 litres

max. operating pressure: 10 bar 70°C max. long-term temperature:

$$p_{ini} = \frac{p_{fin} + 1}{1 + \frac{V_{ex} + V_{K}}{V_{N}} \times \frac{p_{fin} + 1}{p_{0} + 1}} - 1$$

$$p_{ini} = \frac{4,8 + 1}{1 + \frac{2,71 + 18}{60} \times \frac{4,8 + 1}{2,14 + 1}} - 1 = 2,54 \text{ bar}$$

 $p_{_{ini}} \geqq p_{_0} + 0,3 \text{ bar}$ $p_{ini} \ge 2,14 + 0,3 \text{ bar} = 2,44 \text{ bar}$

The required term is fulfilled, the selected elko-flex eder U60-10 can be used.

matching maintenance unit: elko-flex eder maintenance unit 3/4" a/i Note: According to ÖNORM H 5151-1 a pumpcontrolled pressurization device is state of the art in larger systems (nominal power 100 kW and higher, total content 5000 litres and higher or 100 m² solar collector area).

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The nominal volume $V_{N_{min}}$ of these expansion vessels is determined as follows (acc. to EN 12828):

$$V_{\text{N,min}} = (V_{\text{ex}} + V_{\text{WR}}) \times \frac{1}{\eta}$$

SIZING

utilisation efficiency of the expansion vessel η (at pressureless elko-mat eder expansion vessels $\rightarrow \eta = 100 \%$)

Note: In solar systems with a set pressure of 10 bar of the safety valve elko-flex eder U-_10 series expansion vessels can be installed.



Note: The calculation described above follows the standard EN 12828. For a detailed calculation (with determination of the max. vapour volume in case of standstill) the standard ÖNORM M 7777-2 can be applied in Austria.

3.5 Sizing with online design programme elko-online

Explanation of the procedure using the following example:

Determine the appropriate diaphragm expansion vessel for a heating system, which consits of a Biovent C15 and a akku ESP 1000 buffer tank using the online design programme elko-online.

given:

EDEL

power Φ_{NL} of the heat generator = 15 kW $\vartheta_{flow} = 85 \degree C$ $V_{System} = 1.300 I$ $\vartheta_{return} = 65 \degree C$ $h_{st} = 5 \mbox{mWs}$ $\vartheta_{max} = 90 \degree C$ $p_{SV} = 3 \mbox{bar}$

asked for: appropriate expansion vessel necessary gas pressure p₀ within the vessel

- Start the design programme online at: http://elko-online.eder-expansion.at and enter the data of your system (figure 1).
- By clicking the "calculate" button, you are taken to the interim result page. This page shows the results of the calculation and the appropriate products resp. expansion

vessels (figure 2).
3. After selecting the required variant and the suitable accessory click the "finish" button. This opens the result page, where your selected products are summarized. Furthermore it shows the necessary gas pressure for the current system and the appropriate filling pressure of the cold system (figure 3).

<u>Result:</u>

- appropriate expansion vessel: elko-flex eder N 100
- necessary gas pressure p₀:
 p₀ = 0,8 bar

If you want to save your calculation or get a corresponding offer, you need to register at elkoonline. As an unregistered user you can't use these additional functions.

In both cases you can print the result for your further use.



figure 1

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http://elko-online.eder-expansion.at



3.6 Formulary

gas pressure p₀

$$p_0 = p_{st} + 0,2 + p_v$$

total content of the system $V_{\mbox{\tiny System}}$

$$V_{_{System}} = f_{_{an}} \times \Phi_{_{NL}}$$

expansion volume V_{ex}

$$e = 1 - \frac{\rho_{\vartheta max}}{\rho_{\vartheta min}}$$
$$V_{ex} = V_{System} \times e$$

water reserve $V_{\scriptscriptstyle W\!R}$

$$\begin{split} V_{\text{WR}} &= \frac{V_{\text{N}} \times 20}{100} & \text{if } V_{\text{N}} \leq 15 \text{ I} \\ V_{\text{WR}} &= \frac{V_{\text{System}} \times 0.5}{100} \geq 3 & \text{if } V_{\text{N}} > 15 \text{ I} \end{split}$$

minimum set perssure of the safety valve $p_{\scriptscriptstyle SV}$

$$p_{\scriptscriptstyle SV} = p_{\scriptscriptstyle st} + 2 \geqq 3 \, bar$$

closing pressure difference $p_{\scriptscriptstyle SD}$ (acc. to EN ISO 4126-1)

$$p_{\scriptscriptstyle{SD}}$$
 = $p_{\scriptscriptstyle{SV}}\,x\,20~~\%\geqq$ 0,6 bar

final pressure p_{fin}

 $p_{\text{fin}} = p_{\text{SV}} - p_{\text{SD}}$

min. nominal volume of the expansion vessel $V_{N,min}$

$$V_{_{N,min}} = (V_{_{ex}} + V_{_{WR}}) \times \frac{p_{_{fin}} + 1}{p_{_{fin}} - p_{_{0}}}$$

initial pressure $p_{\scriptscriptstyle \text{ini}}$

$$p_{ini} = \frac{p_{fin} + 1}{1 + \frac{V_{ex}}{V_N} \times \frac{p_{fin} + 1}{p_0 + 1}} - 1$$

filling pressure p_{fil}

$$p_{\text{fil}} = V_{\text{N}} \, x \, \frac{p_{\text{o}} + 1}{V_{\text{N}} - V_{\text{System}} \, x \, \left(1 - \frac{\rho_{\text{9fil}}}{\rho_{\text{9min}}}\right) - V_{\text{WR}}} - 1$$

filling pressure $p_{\mbox{\tiny a,min}}$ & $p_{\mbox{\tiny a,max}}$ (acc. to ÖNORM H 5151-1)

$$p_{a,min} = \frac{V_N \times (p_v + 1)}{V_N - V_v} - 1 \qquad \qquad V_v \triangleq V_{WR}$$

$$p_{a,max} = \frac{p_e + 1}{1 + \frac{V_e \times (p_e + 1)}{V_N \times (p_V + 1)}} - 1 \qquad \qquad V_e \triangleq V_{ex}$$
$$p_e \triangleq p_{fin}$$

minimum set pressure of the safety value $\ensuremath{\mathsf{p}_{\text{sv}}}$ in solar systems

$$p_{\scriptscriptstyle SV} = p_{\scriptscriptstyle 0} + 2 \geqq 3 \text{ bar}$$

min. nominal volume of the expansion vessel $V_{\ensuremath{\scriptscriptstyle N,min}}$ in solar systems

$$V_{N,min} = (V_{ex} + V_{K} + V_{WR}) \times \frac{p_{fin} + 1}{p_{fin} - p_{0}}$$

initial pressure $p_{\mbox{\tiny ini}}$ in solar systems

$$p_{\text{ini}} = \frac{p_{\text{fin}} + 1}{1 + \frac{V_{\text{ex}} + V_{\text{K}}}{V_{\text{N}}} x \frac{p_{\text{fin}} + 1}{p_{0} + 1}} - 1$$

- ϑ_{max} maximum set system temperature [°C]
- $\rho_{\mbox{\tiny 9min}}$ density of the medium at the lowest system temperature[kg/m³]
- $\rho_{\scriptscriptstyle \Im\text{max}}$ density of the medium at the maximum set operating temperature [kg/m³]
- $\begin{array}{lll} \rho_{\mbox{\tiny SFI}} & \mbox{density of the medium at the current system} \\ & \mbox{temperature} \left[kg/m^3 \right] \end{array}$
- p_{st} static height pressure [bar]
 10 meter water column (mWs) ~ 1 bar
- p_v vapour pressure (see table 3) [bar]
- $f_{_{an}} \hspace{0.5cm} plant-specific water content (table 1) [\, l/kW\,]$
- $\Phi_{\rm \scriptscriptstyle NL} \quad {\rm max.\,power\,of\,the\,heat\,generator\,[\,kW\,]}$
- e expansion coefficient
- $V_{\kappa} \hspace{0.5cm} total \hspace{0.1cm} content \hspace{0.1cm} of \hspace{0.1cm} the \hspace{0.1cm} collector$

3.7 Tables

table 1:

 $plant-specific water \, content \, f_{{}_{an}}$

system type resp. type of	plant-specific water
heat emitters	content f _{an} [/ kW]
boiler, radiators, UFH	ca. 17
gravitational heating	ca. 17
under floor heating	ca. 17
boiler, sectional radiators	ca. 15
boiler, flat radiators	ca. 13
flow heaters, air heaters	ca. 9
convectors	ca. 9

table 2:

minimum nominal size of the expansion pipe in systems with a nominal power lower than 500 kW acc. to $\ddot{O}NORMH5151-1$

DN	nom. power of the heat generator [kW]
20	up to 120
25	from 120 to 500

The max. flow rate within the expansion pipe must not exceed 0,15 m/s.

table 3:

relative vapour pressure p_v of water and common antifreeze fluids

temperature		relative vapour pressure p _v [bar]					
[°C] water		ethylene glycol			propylene glykol		
		23 % vol. (to -10 °C)	34 % vol. (to -20 °C)	44 % vol. (to -30 °C)	27 % vol. (to -10 °C)	39 % vol. (to -20 °C)	47 % vol. (to -30 °C)
103	0,13	0,04	-	-	0,04	-	-
104	0,17	0,08	0,02	-	0,08	0,02	-
105	0,21	0,11	0,06	-	0,11	0,05	-
106	0,25	0,15	0,09	0,02	0,15	0,09	0,04
107	0,29	0,19	0,13	0,06	0,19	0,13	0,07
108	0,34	0,24	0,17	0,1	0,23	0,17	0,11
109	0,39	0,28	0,21	0,14	0,28	0,21	0,15
110	0,43	0,32	0,25	0,17	0,32	0,25	0,19
120	0,99	0,83	0,74	0,63	0,83	0,74	0,66
130	1,7	1,49	1,36	1,22	1,50	1,36	1,26
140	2,62	2,34	2,16	1,97	2,34	2,16	2,02
150	3,76	3,4	3,17	2,91	3,4	3,17	2,98
160	5,18	4,71	4,42	4,09	4,72	4,42	4,18

table 4:

water content of various pipes

threaded steel tube, medium heavy, welded, acc. to EN 10255			steel tube, welded acc. to EN 10217-1		copper tube acc. to EN 1057	
dimension D _A pipe content		dimension	pipe content	dimension	pipe content	
[mm]	[mm]	[I/m]	[mm]	[I/m]	[mm]	[I/m]
15 (1/2")	21,3	0,20	60,3 x 2,3	2,44	15 x 1	0,13
20 (3/4"	26,9	0,37	76,1 x 2,6	3,95	18 x 1	0,20
25 (1")	33,7	0,58	88,9 x 2,9	5,42	22 x 1	0,31
32 (5/4")	42,4	1,01	114,3 x 3,2	9,14	28 x 1,5	0,49
40 (6/4") 48,3 1,37		139,7 x 36	13,79	35 x 1,5	0,80	



table 5:

density ρ of water and common antifreeze fluids

temperature	density ρ [kg/m³]								
[°C]	water	e	ethylene glyco	bl	р	ropylene glyc	ol		
		23 % vol.	34 % vol.	44 % vol.	27 % vol.	39 % vol.	47 % vol.		
		(to -10 °C)	(to -20 °C)	(to -30 °C)	(to -10 °C)	(to -20 °C)	(to -30 °C)		
-30	983,0	1052	1072	1090	1046	1063	1074		
-25	989,6	1050	1070	1088	1044	1061	1071		
-20	992,8	1049	1068	1086	1042	1058	1068		
-15	995,8	1047	1066	1084	1040	1056	1065		
-10	997,8	1045	1064	1081	1038	1053	1062		
-5	999,1	1043	1062	1079	1036	1050	1059		
0	999,8	1041	1060	1076	1034	1048	1056		
5	999,9	1039	1058	1074	1031	1045	1053		
10	999,8	1037	1055	1071	1029	1042	1050		
15	999,2	1035	1053	1069	1027	1039	1047		
20	998,3	1033	1050	1066	1025	1037	1043		
25	997,1	1030	1048	1063	1022	1034	1040		
30	995,7	1028	1045	1060	1020	1031	1037		
35	994,1	1025	1042	1057	1018	1028	1034		
40	992,2	1023	1040	1054	1015	1025	1030		
45	990,2	1020	1037	1051	1013	1022	1027		
50	988,0	1018	1034	1048	1010	1019	1023		
55	985,7	1015	1031	1045	1008	1016	1020		
60	983,1	1012	1028	1042	1005	1013	1017		
65	980,5	1010	1025	1039	1003	1010	1013		
70	977,7	1007	1022	1035	1000	1006	1009		
75	974,7	1004	1019	1032	997	1003	1006		
80	971,6	1001	1016	1028	995	1000	1002		
85	968,4	998	1012	1025	992	997	999		
90	965,1	995	1009	1021	989	993	995		
95	961,7	992	1005	1018	986	990	991		
100	958,1	988	1002	1014	984	987	987		
105	954,5	985	998	1010	981	983	984		
110	950,7	982	995	1006	978	980	980		
115	940,0 042.0	970	991	1002	975	970	970 072		
120	942,0 038 7	97.5	907	990	972	97.3	972		
120	934.6	968	980	990	966	966	964		
135	930.3	964	976	986	963	962	960		
140	925.9	960	972	982	960	958	956		
145	921.4	957	968	977	956	954	952		
150	916.8	953	964	973	953	951	948		
155	912.1	949	959	969	950	947	944		
160	907.3	945	955	964	947	943	940		
165	902.3	941	951	960	944	939	935		
170	897,3	937	947	955	940	935	931		
175	892,2	932	942	950	937	931	927		
180	886,9	928	938	946	933	928	922		

table 6:

quick selection table for diaphragm expansion vessels in heating systems, valid for: $p_{sv} = 3$ bar, $\vartheta_{max} = 110$ °C

ystem	e	quick selection table for diaphragm expansion vessels valid for set pressure of the safety valve $p_{SV} = 3$ bar, $\vartheta_{max} = 110$ °C								
the sy	volum				gas p	ressure p_0	[bar]			
ent of ªm []	nsion []	0,7	0,8	0,9	1,0	1,1	1,2	1,3	1,4	1,5
conte V _{syste}	expa V _{ex} [minimum	n nominal v	volume V _N	_{min} of the c	diaphragm	expansion [,]	vessel []	
25	1,2	8	9	10	10	11	12	13	14	16
50	2,5	11	12	12	13	14	15	17	19	21
75	3,7	13	14	15	16	17	19	21	23	25
100	4,9	16	17	18	19	21	22	24	27	30
125	6,1	18	19	21	22	24	26	28	31	35
150	7,4	21	22	23	25	27	29	32	35	39
175	8,6	23	25	26	28	30	33	36	39	44
200	9,8	26	27	29	31	34	36	40	44	48
250	12,3	31	32	35	37	40	43	47	52	58
300	14,/	35	38	40	43	46	50	55	60	6/
350	17,2	40	43	46	49	53	5/	62	69	/6
400	19,6	45	48	51	55	59	64	70	//	86
450	22,1	50	53	5/	61	66	71	/8	85	95
500	24,6	55	59	62	6/	72	/8	85	94	104
550	27,0	60 7 E	64 (0	00 74	73	/8 0E	85	93 100	102	113
600	29,5	00 70	09 75	74	/9 0E	85	92	100	120	123
700	31,9	70	75	00	00	92	100	107	120	142
700	34,4	70 Q1	86	00	92	77 106	107	125	129	143
800	30,0	87	92	98	105	113	123	120	1/7	16/
850	/1 7	92	98	10/	112	120	120	1/2	147	17/
900	44.2	97	103	110	118	120	138	151	166	184
950	46.7	103	109	117	125	1.34	146	159	175	194
1000	49.1	108	115	123	131	142	153	167	184	204
1100	54.0	119	126	135	145	156	169	184	202	225
1200	58,9	130	138	147	158	170	184	201	221	245
1300	63,8	141	149	159	171	184	199	217	239	266
1400	68,8	152	161	172	184	198	215	234	258	286
1500	73,7	162	172	184	197	212	230	251	276	307
1600	78,6	173	184	196	210	226	245	268	294	327
1700	83,5	184	195	209	223	241	261	284	313	348
1800	88,4	195	207	221	237	255	276	301	331	368
1900	93,3	206	218	233	250	269	291	318	350	388
2000	98,2	216	230	245	263	283	307	334	368	409
2100	103,1	227	241	258	276	297	322	351	386	429
2200	108,0	238	253	270	289	311	337	368	405	450
2300	113,0	249	264	282	302	325	353	385	423	470
2400	117,9	260	276	294	315	340	368	401	442	491
2500	122,8	271	287	307	329	354	383	418	460	511
2600	127,7	281	299	319	342	368	399	435	478	531
2700	132,6	292	310	331	355	382	414	452	497	552
2800	137,5	303	322	343	368	396	429	468	515	5/2
2900 3000	142,4 147,3	314 325	333 345	356 368	381 394	410	445 460	485 502	534 552	593 613



4. Technical data

4.1 Safety expansion vessels for heating, climatic and cold water systems

elko-flex eder N series

Safety expansion vessels for sealed heating, climatic and cold water systems acc. to EN 12828. Constructed with a non-exchangeable diaphragm to accommodate the expansion volume, gas filling with gas pressure valve, connection for a maintenance unit and single-point mount.

Tested in accordance with Pressure equipment directive (PED) 97/23/EC. max. safety temperature of the system without/with cooling vessel: 90/110 °C max. temperature at the connection point: 70 °C max. operating pressure: 3 bar



N 4 - N 100

type	nom. content [Liter]	standard gas pressure [bar]	D [mm]	T [mm]	t [mm]	connection ["]	weight [kg]	colour
N 4	4	0,8	360	197	80	Rp3/4	3,5	RAL 3001
N 8	8	0,8	360	197	80	Rp3/4	3,5	RAL 3001
N 12	12	0,8	360	197	80	Rp3/4	3,5	RAL 3001
N 18	18	0,8	360	237	80	Rp3/4	3,8	RAL 3001
N 25	25	1,0	400	252	90	Rp3/4	5,0	RAL 3001
N 35	35	1,0	440	290	110	Rp3/4	7,0	RAL 3001
N 50	50	1,0	500	318	145	Rp3/4	10,5	RAL 3001
N 80	80	1,0	600	368	165	Rp3/4	14,5	RAL 3001
N 100	100	1,0	600	433	184	Rp3/4	16,0	RAL 3001

1... connection for expansion pipe (installation in system return, max. long-term temperature at the connection point 70 °C)

2... gas pressure valve with sealing cap and valve protection cap

3... single-point mount

elko-flex eder NP series

Safety expansion vessel, specifically designed for sealed heating systems with buffer tanks, acc. to EN 12828. Constructed with a flanged exchangeable diaphragm to accommodate the expansion volume, gas filling with gas pressure valve and connection for a maintenance unit. Designed as standing vessel with welldesigned and functional stand feet.

Tested in accordance with Pressure equipment directive (PED) 97/23/EC. max. safety temperature of the system without/with cooling vessel: 90/110 °C max. temperature at the connection point: 70 °C max. operating pressure: 3 bar



NP 115 - NP 230

type	nom. content [Liter]	standard gas pressure [bar]	D [mm]	H [mm]	h [mm]	connection ["]	weight [kg]	colour
NP 115	115	1,0	500	750	60	R3/4	30,0	RAL 3001
NP 230	230	1,0	600	1075	60	R3/4	46,0	RAL 3001

1... connection for expansion pipe (installation in system return, max. long-term temperature at the connection point 70 °C)



elko-flex eder SG series

Safety expansion vessel for sealed heating, climatic and cold water systems acc. to EN 12828. Constructed with a flanged exchangeable diaphragm to accommodate the expansion volume, gas filling with gas pressure valve and connection for a maintenance unit. Designed as standing vessel with well-designed and functional stand feet.

Tested in accordance with Pressure equipment directive (PED) 97/23/EC. max. safety temperature of the system without/with cooling vessel: 90/110 °C max. temperature at the connection point: 70 °C max. operating pressure: 3 bar



SG 120 - SG 330

SG 500

type	nom. content	standard gas	D	Н	h	connection	weight	colour
type	[Liter]	pressure [bar]	[mm]	[mm]	[mm]	["]	[kg]	coloui
SG 120	120	1,3	500	790	60	Rp3/4	30,0	RAL 3001
SG 180	180	1,3	500	1080	60	Rp3/4	40,0	RAL 3001
SG 250	250	1,3	600	1090	60	Rp3/4	47,0	RAL 3001
SG 330	330	1,3	600	1340	60	Rp3/4	58,0	RAL 3001
SG 500	500	1,3	600	2090	60	Rp3/4	85,0	RAL 3001

- 1... connection for expansion pipe (installation in system return, max. long-term temperature at the connection point 70 °C)
- 2... gas pressure valve with sealing cap and valve protection cap

elko-flex eder C series

Safety expansion vessel for sealed heating, climatic and cold water systems acc. to EN 12828. Constructed with a flanged exchangeable diaphragm to accommodate the expansion volume, gas filling with gas pressure valve and connection for a maintenance unit (in scope of delivery). Compact design as standing vessel with well-designed and functional stand feet.

Tested in accordance with Pressure equipment directive (PED) 97/23/EC. max. safety temperature of the system without/with cooling vessel: 90/110 °C max. temperature at the connection point: 70 °C max. operating pressure: 3 bar



C 600 - C 1000

type	nom. content [Liter]	standard gas pressure [bar]	D [mm]	H [mm]	h [mm]	connection ["]	weight [kg]	colour
C 600	600	1,3	700	1990	65	R1	95,0	RAL 3001
C 800	800	1,3	800	2000	50	R1	104,0	RAL 3001
C 1000	1000	1,3	900	2050	75	R1	135,0	RAL 3001

1... connection for expansion pipe (installation in system return, max. long-term temperature at the connection point 70 °C)



elko-flex eder CV series

Safety expansion vessel for sealed heating, climatic and cold water systems acc. to EN 12828. Constructed with a flanged exchangeable diaphragm to accommodate the expansion volume, gas filling with gas pressure valve and connection for a maintenance unit (in scope of delivery). Compact and reinforced design as standing vessel with well-designed and functional stand feet.

Tested in accordance with Pressure equipment directive (PED) 97/23/EC. max. safety temperature of the system without/with cooling vessel: 90/110 °C max. temperature at the connection point: 70 °C max. operating pressure: 5 bar



CV 120 - CV 330

CV 600

t) (D 0	nom. content	standard gas	D	Н	h	connection	weight	colour
type	[Liter]	pressure [bar]	[mm]	[mm]	[mm]	["]	[kg]	colour
CV 120	120	3,3	500	860	50	R3/4	40,0	RAL 3001
CV 180	180	3,3	500	1185	50	R3/4	55,0	RAL 3001
CV 250	250	3,3	600	1195	60	R3/4	73,0	RAL 3001
CV 330	330	3,3	600	1395	60	R3/4	84,0	RAL 3001
CV 600	600	3,3	700	1990	50	R1	161,0	RAL 3001

- 1... connection for expansion pipe (installation in system return, max. long-term temperature at the connection point 70 °C)
- 2... gas pressure valve with sealing cap and valve protection cap

4.2 Universal vessels for heating, climatic and cold water systems

elko-flex eder U_-6 series

Universal safety expansion vessel for sealed heating, climatic and cold water systems acc. to EN 12828, refrigeration systems, solar systems and cold water sanitary systems. Non-flow-through construction with a flanged exchangeable diaphragm (resistant to common antifreeze fluids, the flange is made of stainless steel) to accommodate the expansion volume, gas filling with gas pressure valve and connection for a maintenance unit. Designed for wall mount installation incl. functional mounting bracket (18 - 50 l) resp. as standing vessel with well-designed and functional stand feet (90 - 300 l).

Tested in accordance with Pressure equipment directive (PED) 97/23/EC. max. temperature at the connection point: 70 $^\circ\rm C$

max. operating pressure: 6 bar



type	nom. content	standard gas	D	Н	t/h	connection	weight	colour
-)	[Liter]	pressure [bar]	[mm]	[mm]	[mm]	["]	[kg]	
U18-6	18	3,5	300	365	230	R3/4	7,9	RAL 3001
U25-6	25	3,5	360	400	230	R3/4	9,8	RAL 3001
U35-6	35	3,5	360	500	230	R3/4	10,5	RAL 3001
U50-6	50	3,5	360	580	230	R3/4	14,8	RAL 3001
U90-6	90	3,5	440	820	85	R1	31,3	RAL 3001
U120-6	120	3,5	500	835	85	R1	40,5	RAL 3001
U200-6	200	3,5	500	1260	85	R1	56,0	RAL 3001
U300-6	300	3,5	600	1400	85	R1	81,4	RAL 3001

1... connection for expansion pipe (installation in system return, max. long-term temperature at the connection point 70 °C)



elko-flex eder U_-10 series

Universal safety expansion vessel for sealed heating, climatic and cold water systems acc. to EN 12828, refrigeration systems, solar systems and cold water sanitary systems. Non-flow-through construction with a flanged exchangeable diaphragm (resistant to common antifreeze fluids, the flange is made of stainless steel) to accommodate the expansion volume, gas filling with gas pressure valve and connection for a maintenance unit. Designed for wall mount installation incl. functional mounting bracket (15 - 60 l) resp. as standing vessel with well-designed and functional stand feet (120 - 300 l).

Tested in accordance with Pressure equipment directive (PED) 97/23/EC. max. temperature at the connection point: 70 °C max. operating pressure: 10 bar



type	nom. content [Liter]	standard gas pressure [bar]	D [mm]	H [mm]	t / h [mm]	connection ["]	weight [kg]	colour
U15-10	15	3,5	300	310	230	R3/4	6,1	RAL 3001
U20-10	20	3,5	300	360	230	R3/4	6,7	RAL 3001
U30-10	30	3,5	360	420	230	R3/4	9,6	RAL 3001
U60-10	60	3,5	360	695	230	R3/4	15,8	RAL 3001
U120-10	120	3,5	500	870	75	R1	30,0	RAL 3001
U180-10	180	3,5	500	1180	80	R1	55,0	RAL 3001
U240-10	240	3,5	600	1195	80	R1	73,0	RAL 3001
U300-10	300	3,5	600	1400	80	R1	84,0	RAL 3001

1... connection for expansion pipe (installation in system return, max. long-term temperature at the connection point 70 °C)

Expansion vessels for warm water sanitary systems 4.3

elko-san eder San D series

Safety expansion vessel for warm water sanitary systems. Constructed with a flanged exchangeable diaphragm (made of food-safe and tasteless material, the flange is made of stainless steel) to accommodate the expansion volume (caused by heating-up of the water boiler), gas filling with gas pressure valve and - for flow-through - connections for two maintenance units. Designed for wall mount installation incl. functional mounting bracket (20-60 l) resp. as standing vessel with well-designed and functional stand feet (90-300 l).

Tested in accordance with Pressure equipment directive (PED) 97/23/EC. max. temperature at the connection point: 70 °C max. operating pressure: 10 bar



San 20 D - San 60 D

type	nom. content [Liter]	standard gas pressure [bar]	D [mm]	H [mm]	t / h [mm]	connection	weight [ka]	colour
	[=	le : e e e e e e e e e e e e e e e e e e	[]	[]	[]		1	
San 20 D	20	3,5	300	410	230	R3/4	6,9	RAL 5015
San 30 D	30	3,5	360	445	230	R3/4	11,0	RAL 5015
San 60 D	60	3,5	360	715	230	R3/4	16,4	RAL 5015
San 90 D	90	3,5	440	900	90	R1	32,6	RAL 5015
San 120 D	120	3,5	500	900	80	R1	35,0	RAL 5015
San 180 D	180	3,5	500	1220	80	R1	60,0	RAL 5015
San 240 D	240	3,5	600	1235	80	R1	78,0	RAL 5015
San 300 D	300	3,5	600	1440	80	R1	89,0	RAL 5015

1... connection FROM the system

- 2... connection TO the system
- gas pressure valve with sealing cap and valve protection cap 2...



4.4 Expansion vessels for cold water sanitary systems

elko-san eder San series

Safety expansion vessel for cold water sanitary systems to absorb pressure surges or as water pressure tanks. Constructed with a flanged exchangeable diaphragm (made of food-safe and tasteless material, the flange is made of stainless steel), gas filling with gas pressure valve and connection for a maintenance unit. Designed for wall mount installation incl. functional mounting bracket (15 - 60 l) resp. as standing vessel with well-designed and functional stand feet (120 - 300 l).

Tested in accordance with directive 97/23/EC (PED). max. temperature at the connection point: 70 °C max. operating pressure: 10 bar **Caution:** elko-san eder San series expansion vessels are not intended as shock absorbers in their proper sense!



1... connection for expansion pipe (max. long-term temperature at the connection point 70 °C)

4.5 Safety expansion vessel for refrigeration systems (cold water systems, chillers)

elko-flex eder Cool series

Safety expansion vessel for refrigeration systems. Constructed with a flanged exchangeable diaphragm (resistant to common antifreeze fluids, the flange is made of stainless steel) to accommodate the expansion volume, gas filling with gas pressure valve and connection for a maintenance unit. Designed for wall mount installation incl. functional mounting bracket.

Tested in accordance with Pressure equipment directive (PED) 97/23/EC. max. temperature at the connection point: 70 °C min. temperature at the connection point: -10 °C max. operating pressure: 6 bar



Cool 18 - Cool 50

type	nom. content [Liter]	standard gas pressure [bar]	D [mm]	H [mm]	t [mm]	connection ["]	weight [kg]	colour
Cool 18	18	3,5	300	365	230	R3/4	7,9	RAL 7035
Cool 25	25	3,5	360	400	230	R3/4	9,8	RAL 7035
Cool 35	35	3,5	360	500	230	R3/4	10,5	RAL 7035
Cool 50	50	3,5	360	580	230	R3/4	14,8	RAL 7035

1... connection for expansion pipe to the cold water system



4.6 Safety expansion vessel for solar system

elko-flex eder Solar series

Safety expansion vessel for solar systems. Constructed with a flanged exchangeable diaphragm (resistant to common antifreeze fluids, the flange is made of stainless steel) to accommodate the expansion volume, gas filling with gas pressure valve and connection for a maintenance unit. Designed for wall mount installation incl. functional mounting bracket (18 - 50 l) resp. as standing vessel with well-designed and functional stand feet (90 - 300 l).

Tested in accordance with directive 97/23/EC (PED). max. temperature at the connection point: 70 °C max. operating pressure: 6 bar **Note:** The U_-6 series can be used as an alternative to the Solar series. For solar systems up to max. 10 bar the U_-10 series can be installed.



type	nom. content [Liter]	standard gas pressure [bar]	D [mm]	H [mm]	t / h [mm]	connection ["]	weight [kg]	colour
Solar 18	18	3,5	300	365	230	R3/4	7,9	RAL 6010
Solar 25	25	3,5	360	400	230	R3/4	9,8	RAL 6010
Solar 35	35	3,5	360	500	230	R3/4	10,5	RAL 6010
Solar 50	50	3,5	360	580	230	R3/4	14,8	RAL 6010
Solar 90	90	3,5	440	820	85	R1	31,3	RAL 6010
Solar 120	120	3,5	500	835	85	R1	40,5	RAL 6010
Solar 200	200	3,5	500	1260	85	R1	56,0	RAL 6010
Solar 300	300	3,5	600	1400	85	R1	81,4	RAL 6010

1... connection for expansion pipe to the solar system

ACCESSORY

5. Accessory

EDEL

5.1 elko-flex eder maintenance unit

An elko-flex eder maintenance unit is a connection accessory for diaphragm expansion vessels for approved integration into a system with all necessary maintenance functions.

To ensure a proper function of the vessel and the whole system for a long term expansion vessels with a constant primary pressure habe to be checked regularly (recommended every year, but at least every 2 years). Though the gas pressure in the vessel in the water-sided, pressureless condition is proved and corrected if necessary.

The vessel has to be separated from the system by an armature and to be emptied.

Excerpt of standard EN 12828: During operation the connection between the pressurization system and the heat generator has to be permanently ooen. For maintenance it is recommended to build in a valve between the pressurization system and the heat generator. The valve has to be secured against unintended closing, equipped with a drainage valve and used as a shut-off device.

Excerpt of standard ÖNORM H 5151-1: Between expansion- or pressurization system and heat generator maintenance and exchange of expansion- or pressurization devices has to be enabled by suitable equipment.

Technical data: max. operating pressure: 10 bar max. operating temperature: 95 °C

type	connection to system ["]	conneciton to vessel ["]	length [mm]
3/4" a/a	R3/4	R3/4	104
3/4" a/i	R3/4	Rp3/4	87
1" a/i	R1	Rp1	101

type overview elko-flex eder maintenance unit:



5.2 elko-mat eder EV cooling vessel

EV cooling vessels are intended for cooling the expansion volume before it enters the safety expansion vessel. Therefore the safety expansion vessel is protected against too high temperatures.

EV cooling vessels must be provided if the temperature at the connection point exceeds the max. allowed temperature of 70 °C

max. operating temperature (=safeety temperature) of the system: 110 °C

Special versions of EV cooling vessels for operating temperatures higher than 110 °C can be delivered on request.

example: elko-flex eder safety expansion vessel with EV cooling vessel:



Better heating.

EDEL

5.3 elko-flex eder SV safety valve elko-mat eder SV safety valve

To ensure that the maximum operating pressure is not exceeded, each heat generator of a heating system has to be assured by a safety valve.

The safety valve must be installed as close as possible to the heat generator - as long as the heat generator is not equipped with a safety valve ex works.

Safety valves shall:

- have a minimum dimension of DN15
- open at a pressure which does not exceed the maximum operating pressure of the system. Further it must avoid an exceeding of more than 10 % of the max. operating pressure. In case of a max. operating pressure of not more than 3 bar an exceeding of 0,5 bar is admissible.
- be designed in a way that the pressure loss does not exceed 3 % in the inlet pipe and 10 % in the outlet, compared to the set pressure of the safety valve.
- be installed at an easy accessible position and as close as possible to the flow pipe of the heat generator. Between the heat generator and the safety valve no shut-off device must be installed!

Safety valves should be dimensioned and set so that the operating overpressure in normal heating operation resp. in case of failure cannot be exceeded by more than 10%. When the operating overpressure is below 3 bar, a pressure in excess of maximal 0,3 bar is admissible. The safety valves should close when the pressure drops within a range of 10% of the response overpressure. A pressure reduction of 0,3 bar is admissible with response overpressures below 3 bar.

4.3.1 Selection of the safety valve:

To select a suitable safety valve the following technical specifications are necessary:

- nominal power of the heat generator
- set pressure of the safety valve $p_{\scriptscriptstyle SV}$

static height h _{st} of the heating system [mWs]	min. set pressure p _{sv} [bar]		
h _{st} ≤ 10	3,0		
h _{st} > 10	p _{st} + 2,0		

The selection of the safety valves based on their relief capacity depends on their type-examination.

The relief capacities of elko-flex eder SV resp.. elko-mat eder SV safety valves are summarized in table 7.

table 7:

 ${\sf Relief\,capacities\,of\,elko-flex\,eder\,SV/elko-mat\,eder\,SV\,safety\,valves}$

set pressure p _{SV} [bar]	relief capacity of the safety valve [kW] in reference to the inlet dimension and the set pressure p _{SV}						
	DN15 (1/2")	DN20 (3/4")	DN25 (1")	DN32 (5/4")	DN40 (6/4")	DN50 (2")	
3	50	100	200	350	600	900	
4	undeliverable	undeliverable	200	350	600	900	
5	undeliverable	undeliverable	200	350	600	900	
6	75	150	250	350	600	900	
8	undeliverable	undeliverable	250	350	600	900	
10	undeliverable	undeliverable	250	350	600	900	





ANTON EDER GMBH

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